



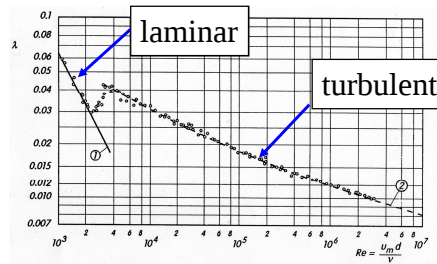
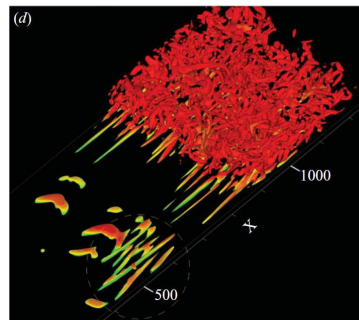
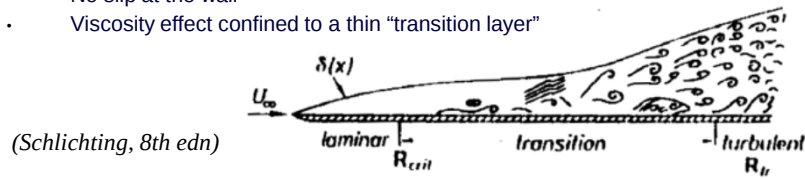
Plan

1. Basic knowledge of boundary layers
2. Statistical quantities
3. Wall-bounded flows simulations
4. A glimpse at high-Reynolds number wall-bounded flows
5. Applications

Laminar/turbulent boundary layer

L. Prandtl, 1904, Heidelberg

- No slip at the wall
- Viscosity effect confined to a thin “transition layer”



Transition visualisation (Wu & Moin, JFM 2009)

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Remarks

- Turbulent flows are very different from their laminar counterpart:
 - Increased skin friction/pressure loss
 - Increased BL thickness
 - Increased heat/mass transfer properties
 - → technological importance!
- What are the associated physical mechanisms?
- Understanding is required to design/optimize systems and control devices

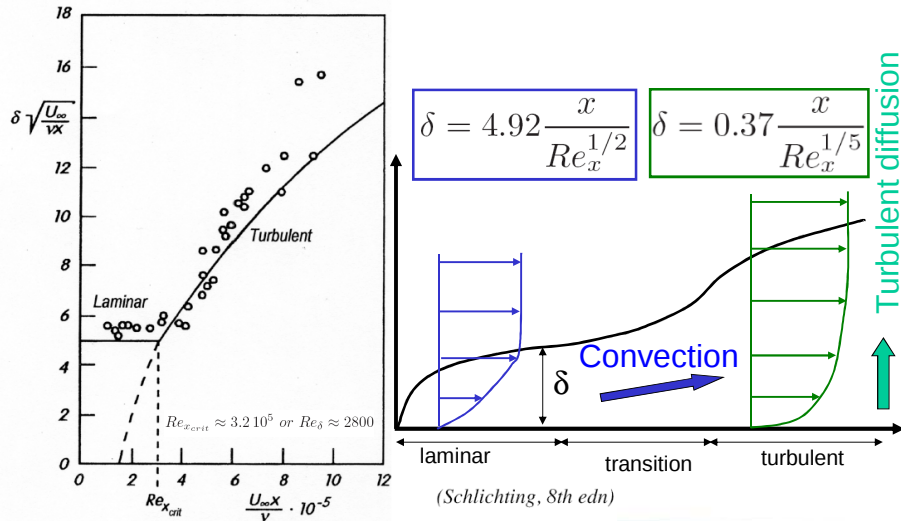
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1. Introductory concepts: a glimpse at diffusion (cont'd)

- Growth of a flat plate boundary layer



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Global parameters (1/3)

Skin friction coefficient

$$C_f = \frac{\tau_p}{1/2 \rho U_\infty^2} \quad u_\tau = \sqrt{\tau_p / \rho} \quad (\Rightarrow C_f / 2 = u_\tau^2 / U_\infty^2)$$

Boundary layer thickness based Reynolds number

$$Re_\delta = \delta U_\infty / \nu \quad Re_\tau = \frac{\delta u_\tau}{\nu} = \delta^+$$

Displacement and Rotta-Clauser thicknesses

$$\Delta = \frac{U_\infty}{u_\tau} \delta_1 = \int_0^\infty \frac{U_\infty - \langle u \rangle}{u_\tau} dy$$

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Global parameters (2/3)

Momentum thickness

$$\theta = \int_0^\infty \frac{\langle u \rangle}{U_\infty} \left(1 - \frac{\langle u \rangle}{U_\infty}\right) dy \longrightarrow Re_\theta = \frac{\theta U_\infty}{\nu}$$

$$C_f/2 = d\theta/dx$$

Shape factor

$$H = \delta_1/\theta$$

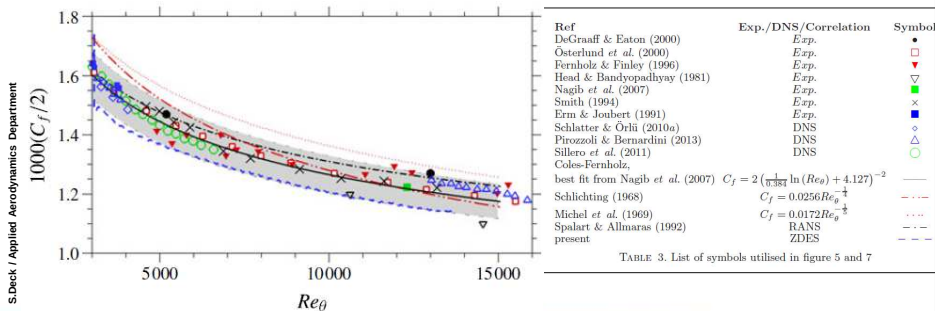
Turbulent: H=1.3-1.4

Laminar: H=2.59

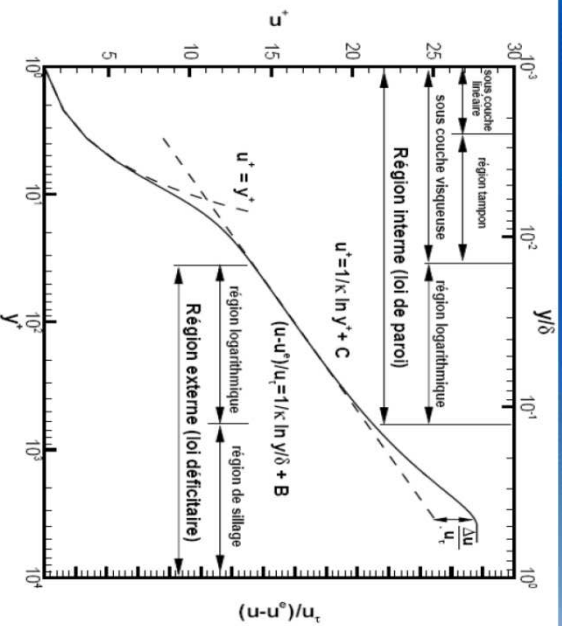
Global parameters (3/3)

	C_f	θ/x	δ_1/x	δ/x
Laminaire, Blasius	$0.664 \cdot Re_x^{-1/2}$	$0.664 \cdot Re_x^{-1/2}$	$1.721 \cdot Re_x^{-1/2}$	$4.92 \cdot Re_x^{-1/2}$
Turbulent, loi en 1/7 [49]	$0.0594 \cdot Re_x^{-1/5}$	$0.037 \cdot Re_x^{-1/5}$	$0.0477 \cdot Re_x^{-1/5}$	$0.38 \cdot Re_x^{-1/5}$
Turbulent, Michel [49]	$0.0368 \cdot Re_x^{-1/6}$	$0.0221 \cdot Re_x^{-1/6}$	$0.0309 \cdot Re_x^{-1/6}$	

	C_f	θ/x	δ_1/x	δ/x
Laminaire, Blasius	$0.441 \cdot Re_\theta^{-1}$	$0.441 \cdot Re_\theta^{-1}$	$1.143 \cdot Re_\theta^{-1}$	$3.268 \cdot Re_\theta^{-1}$
Turbulent, loi en 1/7 [49]	$0.026 \cdot Re_\theta^{-1/4}$	$0.0163 \cdot Re_\theta^{-1/4}$	$0.0209 \cdot Re_\theta^{-1/4}$	$0.167 \cdot Re_\theta^{-1/4}$
Turbulent, Michel [49]	$0.0172 \cdot Re_\theta^{-1/5}$	$0.0103 \cdot Re_\theta^{-1/5}$	$0.0144 \cdot Re_\theta^{-1/5}$	



Mean Velocity



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Reynolds stresses (1/3)

$$\partial_t \langle u'^2 \rangle + \langle u \rangle \partial_x \langle u'^2 \rangle + \langle v \rangle \partial_y \langle u'^2 \rangle = \boxed{2P} + A_u + D_{ru} + C_u - D_{eu}$$

$$P = -\langle u'v' \rangle \partial_y \langle u \rangle$$

$$A_u = -2\langle u'^2 \rangle \partial_x \langle u \rangle$$

$$D_{ru} = \partial_y (-\langle \tilde{v} u'^2 \rangle + \nu \partial_y \langle u'^2 \rangle)$$

$$C_u = 2\langle \tilde{p} / \rho \partial_x u' \rangle$$

$$D_{eu} = 2\nu \langle \partial_{x_i} u' \partial_{x_i} u' \rangle$$

$$\partial_t \langle v'^2 \rangle + \langle u \rangle \partial_x \langle v'^2 \rangle + \langle v \rangle \partial_y \langle v'^2 \rangle = (A_v) + D_{rv} + C_v - D_{ev}$$

$$D_{rv} = \partial_y (-\langle \tilde{v}^3 \rangle - 2\langle \tilde{p} / \rho v' \rangle + \nu \partial_y \langle v'^2 \rangle)$$

$$C_v = 2\langle \tilde{p} / \rho \partial_y v' \rangle$$

$$D_{ev} = 2\nu \langle \partial_{x_i} v' \partial_{x_i} v' \rangle$$

$$\partial_t \langle w'^2 \rangle + \langle u \rangle \partial_x \langle w'^2 \rangle + \langle v \rangle \partial_y \langle w'^2 \rangle = D_{rw} + C_w - D_{ew}$$

$$D_{rw} = \partial_y (-\langle \tilde{v} w'^2 \rangle + \nu \partial_y \langle w'^2 \rangle)$$

$$C_w = 2\langle \tilde{p} / \rho \partial_z w' \rangle$$

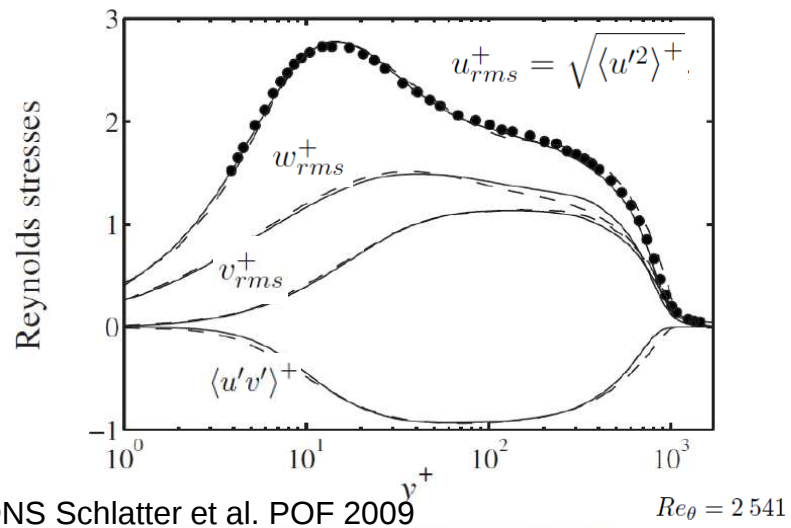
$$D_{ew} = 2\nu \langle \partial_{x_i} w' \partial_{x_i} w' \rangle$$

$$C_u + C_v + C_w = 0;$$

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Reynolds stresses (2/3)

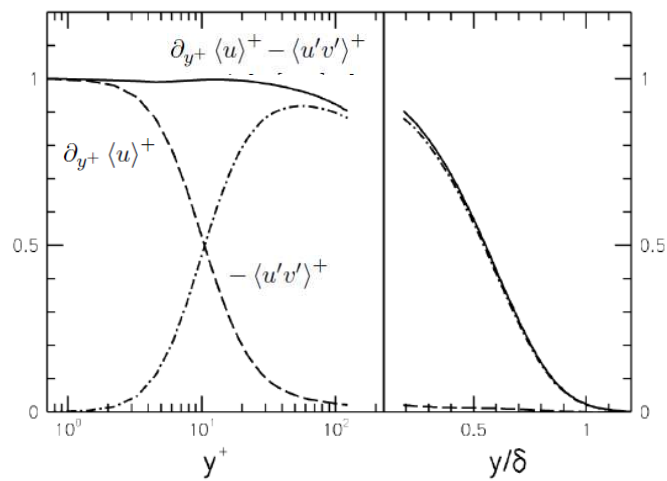


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Reynolds stresses (3/3)



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3. Statistical description in real space: Turbulent Kinetic Energy (TKE) equation.

Setting $i=j$ in the Reynolds stress equation yields:

$$\frac{d}{dt}(\rho \bar{k}) = \underbrace{-\rho \overline{u'_i u'_k} \frac{\partial \bar{U}_i}{\partial x_k}}_{\text{p.P: Transfert term (production)}} + \underbrace{\tau'_{ik} \frac{\partial u'_i}{\partial x_k}}_{\text{Rate of dissipation}} - \underbrace{\frac{1}{2} \frac{\partial}{\partial x_k} [\rho \overline{u'_i u'_i u'_k}]}_{\text{Turbulent diffusion}} - \underbrace{u'_i \frac{\partial p'}{\partial x_i}}_{\text{Pressure diffusion}} + \underbrace{\frac{\partial}{\partial x_k} [\overline{u'_i \tau'_{ik}}]}_{\text{Viscous diffusion}}$$

→ Note that the term which transfers energy from the mean flow to turbulence appears in both mean and fluctuating KE equation but with an opposite sign
 → This latter term represents now the rate at which energy enters the turbulence and passes through the cascade

Rate of dissipation of TKE

$$\rho \epsilon \equiv \overline{\tau'_{ik} \frac{\partial u'_i}{\partial x_k}} = 2\mu \overline{s_{ij}^2} = \frac{1}{2}\mu \left(\frac{\partial u'_i}{\partial x_j} + \frac{\partial u'_j}{\partial x_i} \right)^2 \geq 0 \quad (\epsilon \sim \text{m}^2 \cdot \text{s}^{-3})$$

→ The rate at which energy is dissipated in regions where the instantaneous velocity gradients are large e.g. in the smallest eddies

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3. Statistical description in real space: Turbulent Kinetic Energy (TKE) equation (cont'd).

- Interpretation of $P \equiv -\rho \overline{u'_i u'_j} \frac{\partial \bar{U}_i}{\partial x_j}$. This term vanishes in the equation of the total (mean+fluctuating) kinetic energy.
 → exchange term of energy between the mean flow and turbulence

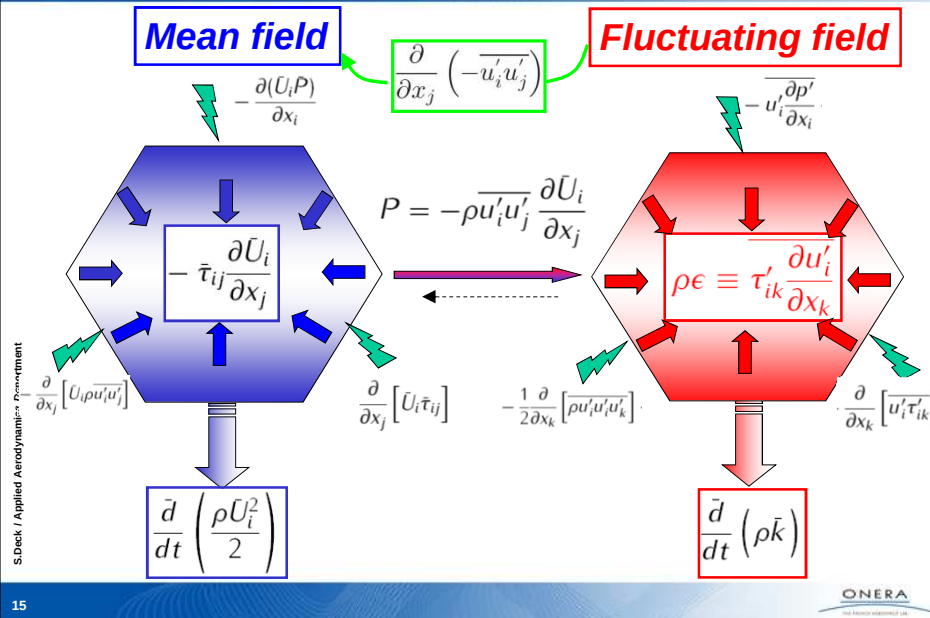
$$P = -\rho \overline{u'_i u'_j} \bar{S}_{ij}$$

- In most turbulent flows, $P = -\rho \overline{u'_i u'_j} \frac{\partial \bar{U}_i}{\partial x_j} > 0$

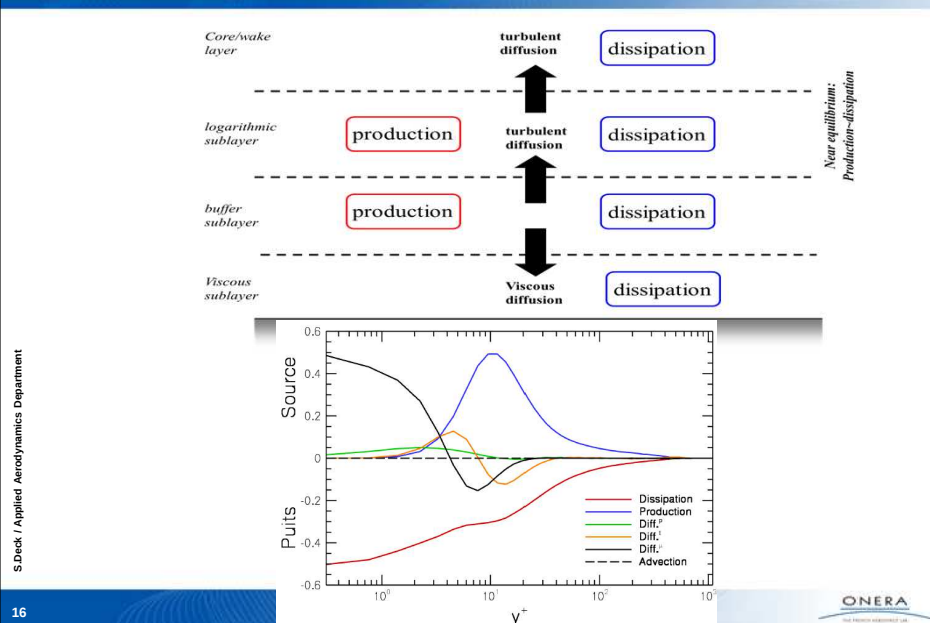
→ production of turbulent energy by working of the mean flow on the turbulent Reynolds stresses.

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3. The exchange of energy between the mean flow and turbulence (cont'd).

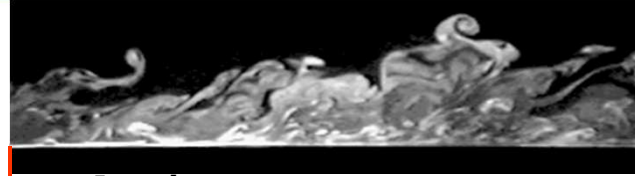


Turbulent Kinetic Energy



Turbulent Boundary Layer Structure

Wall-bounded flows: the 2-scale problem



Inner layer

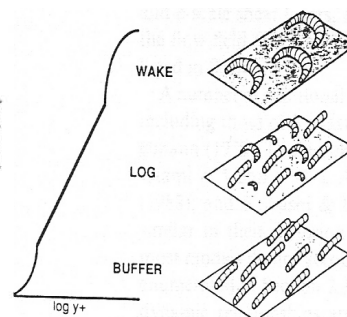
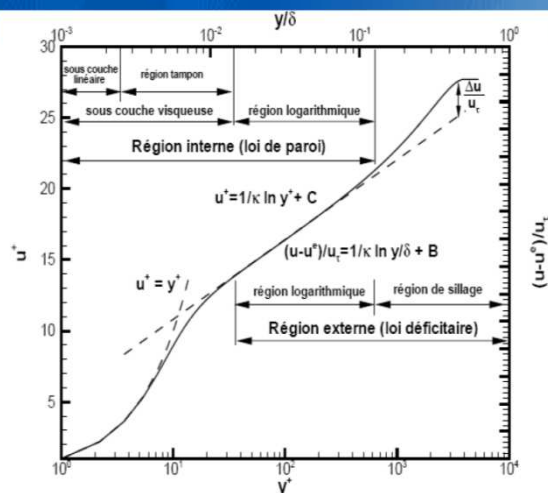
- Production
- Dissipation
- Structures: streaks

Outer layer

- Dissipation
- Structure size $\sim \delta_{99}$

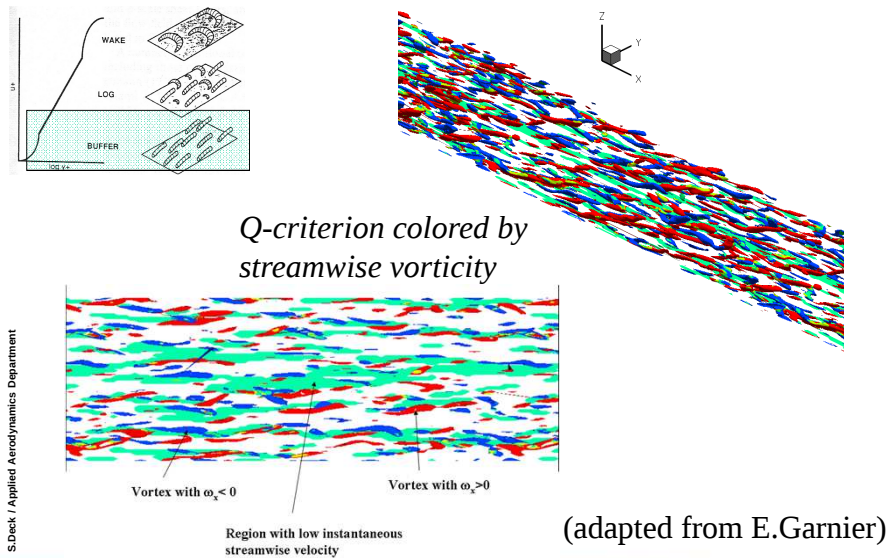
- Near a (smooth) wall, viscous mechanisms give rise to a viscosity based length scale (where u' is a characteristic turbulent velocity scale) $l_v \propto \nu/u'$
- The near wall dynamics (in the **wall/inner layer**) must be dominated by structures of this size
- The second « natural » (large) scale is the boundary layer thickness (or the pipe radius) δ_{99} . Structures of this size should govern the dynamics far from the wall (in the **outer layer**)
- one expects from the existence of two regions an asymptotically matching in an intermediary **inertial layer**

Turbulent Boundary Layer Structure



- The dynamics is associated with a very complex instantaneous flow organization
- Several types of flow structures are observed
- Each layer exhibits different coherent events
- Identification of the exact role of each structure is still an open controversial issue

Viscous and buffer layer



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Viscous and buffer layer

- Low/high-speed Streamwise velocity streaks: sinuous arrays of alternating streamwise jets superimposed on the mean shear (*Kim & al., 1971*)
 - Average spanwise wavelength $z+=50-100$ (*Smith & al., 1983*)
 - Average streamwise length $x+=1000$
 - Wall shear is higher than the average at locations where the jets point forward (resp. backward) for high speed (resp. low speed) streaks
- Quasi-streamwise vortices
 - Slightly tilted from the wall (9 degrees)
 - Stay in the near-wall region only for $x+=200$ (*Jeong & al., 1997*)
 - Have a diameter ranging from 10 to 40+
 - Several vortices are associated with each streak, with longitudinal spacing $x+=400$
 - Some of them are connected to legs of hairpin vortices in the log layer, but most merge in incoherent vorticity away from the wall
 - Are advected at speed $c+=10$

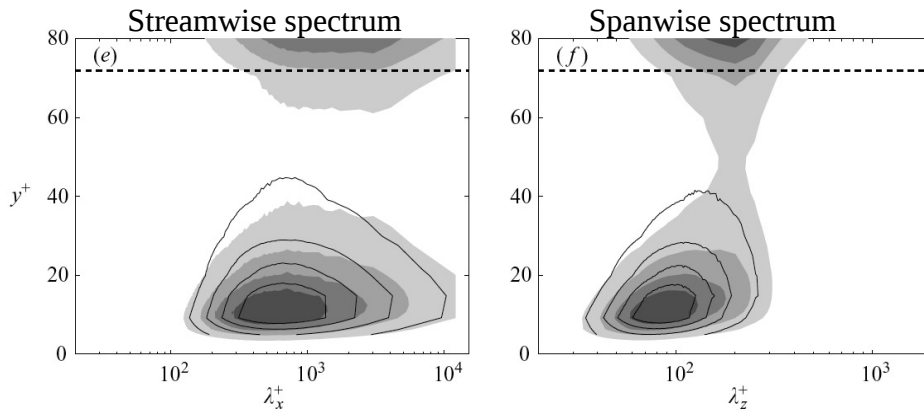
(adapted from E.Garnier)

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Viscous and buffer layer. Spectral analysis of TKE production



Conclusion: TKE production concentrated

(Jimenez & al., 2004)

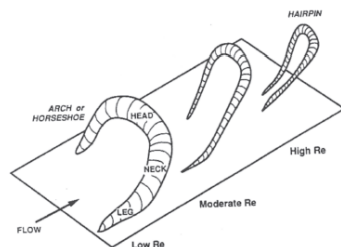
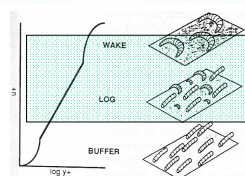
- below $y^+ = 30$,
- around $\lambda_x^+ \approx 600$ and $\lambda_z^+ \approx 100$

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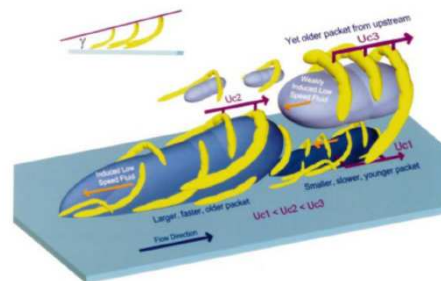
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Log/wake region



Re dependence of the hairpin shape. *Robinson 1991*

Triggering of the outer cycle by the inner one



BL dynamics explained by hairpin packets. *Adrian JFM 2000*

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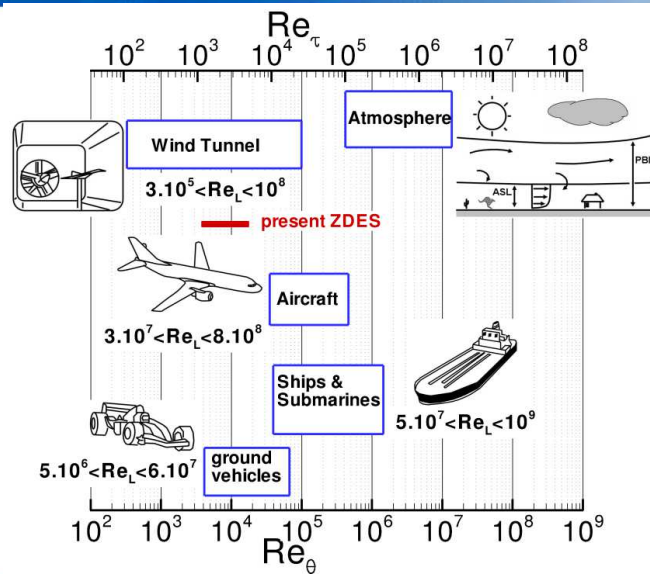
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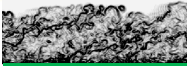
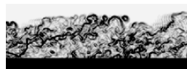
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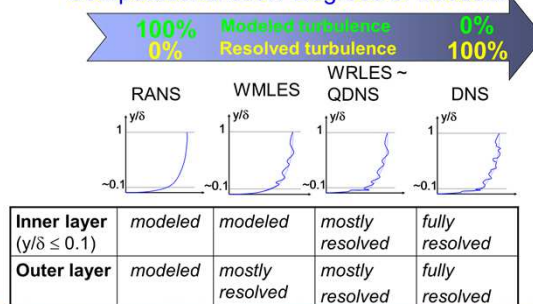
Computational cost



Computational cost

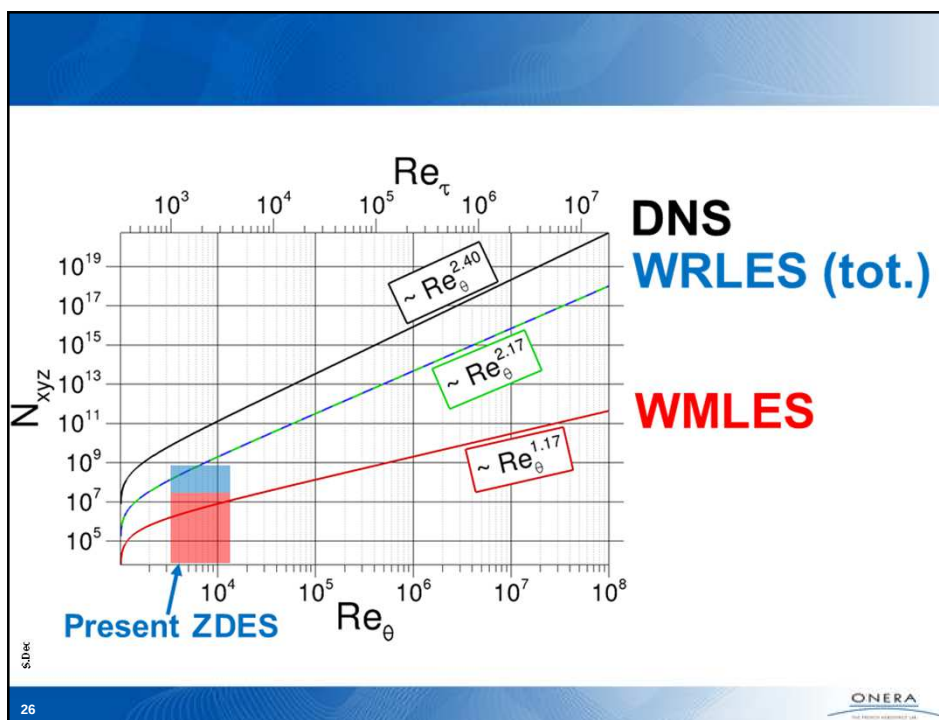
- Direct Numerical Simulation (**DNS**) : prohibitive 
- Wall-Resolved Large Eddy Simulation (**WRLES**): Quasi-DNS (**inner zone**)
- Wall-Modelled LES (**WMLES**) : affordable at high Reynolds numbers (**modelled inner zone**) 

Computational cost / Degrees of freedom



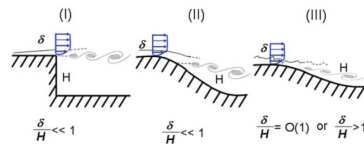
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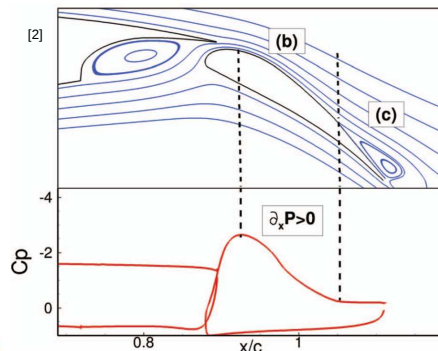


Wall-bounded turbulence-resolving simulations

- **Average** statistical description: **RANS** (**Reynolds-Averaged Navier-Stokes**)
- **Turbulence-resolving**:
 - Flow dominated by **history of upstream** boundary layer
 - Applications (**unsteady loads, aeroacoustics...**)

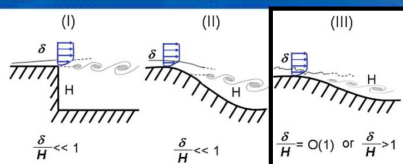


[1] Deck S., Recent improvements in the Zonal Detached Eddy Simulation (ZDES) formulation, *Theoretical Computational Fluid Dynamics*, 2012, 26, 523-550.



Winkler et al., Direct Numerical Simulation of the self-noise radiated by an airfoil in a narrow stream, AIAA 2012-2059

Zonal Detached Eddy Simulation (ZDES)



ZDES Mode III:
Wall-Modelled LES,
Wall-Resolved LES capability ([3])



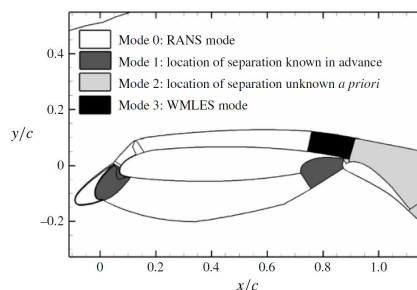
- **Multi-resolution hybrid RANS/LES technique**
- Ranging from RANS to **WRLES**, extensive **validation basis**

[1] Deck S., Recent improvements in the Zonal Detached Eddy Simulation (ZDES) formulation, *Theoretical Computational Fluid Dynamics*, 2012, 26, 523-550.

Deck S., Gand F., Brunet V. & Khelil S. B., High-fidelity simulations of unsteady civil aircraft aerodynamics: stakes and perspectives. Application of Zonal Detached Eddy Simulation (ZDES), *Philosophical Transactions of the Royal Society A*, 2014, 372:20130325.

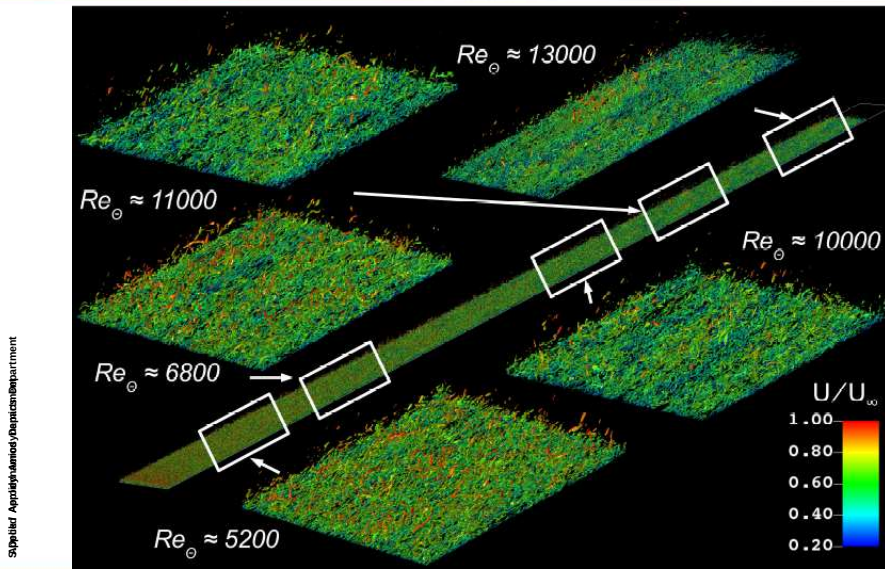
[3] Deck S., Renard N., Laraufige R. and Weiss P.-E., Large scale contribution to mean wall shear stress in high Reynolds number flat plate boundary layers up to $Re_\tau=13650$, *Journal of Fluid Mechanics*, 2014, 743, 202-248

[4] Deck S., Renard N., Laraufige R. and Sagaut P., Zonal Detached Eddy Simulation of a spatially developing flat plate turbulent boundary layer over the Reynolds number range $3150 \leq Re_\tau \leq 14000$, *Physics of Fluids*, 2014, 26, 025116



Deck, S. & Laraufige, R., Numerical investigation of the flow dynamics past a three-element airfoil, *Journal of Fluid Mechanics*, 2013, 732, 401-444

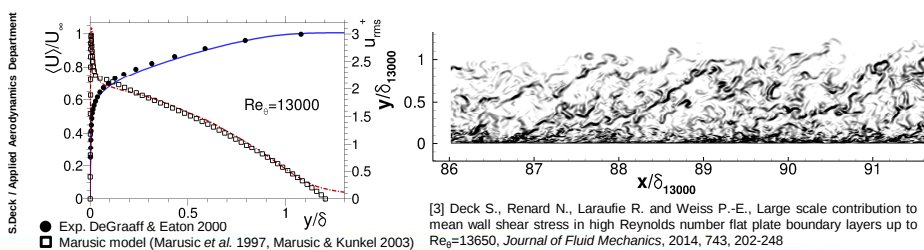
GENCI: projet ZDESWALLTURB



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Wall-Resolved Large Eddy Simulation database

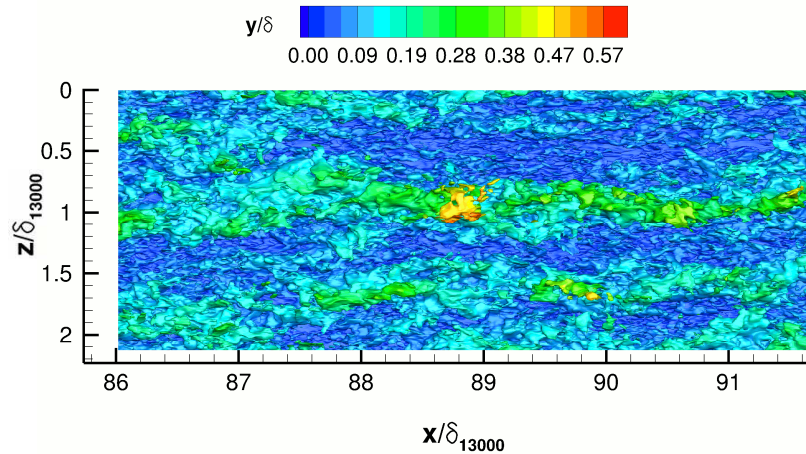
- WRLES of a **spatially developing** zero-pressure-gradient flat-plate turbulent **boundary layer**
- $3060 \leq Re_\theta \leq 13650$, $L_x = 342 \delta_0$, $M_\infty = 0.21$
- **ZDES mode III**, $\Delta x^+ = 50$, $\Delta z^+ = 12$, $N_{xyz} = 800 \cdot 10^6$
- **2.10⁶ CPU hours** on **936** Nehalem processors of the CINES superscalar computer Jade-SGI Altix Ice 8200, **GENCI** project ZDESWALLTURB, **3 Terabytes** of data
- Low-dissipative AUSM+(P), FV, 2nd order implicit time integration



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Flow visualization

• $Re_\theta \approx 13000$, $u^+ = 20$

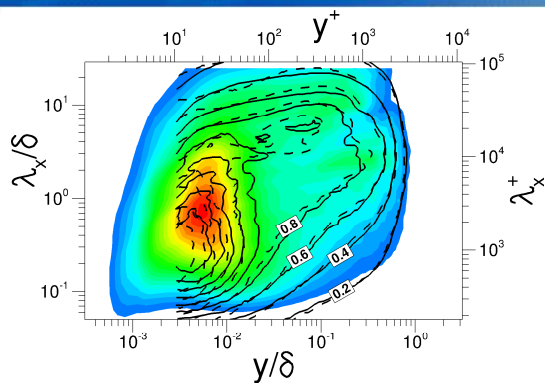


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Streamwise PSD of u' at $Re_\theta = 13000$



$k_x G_{uu} / u_\tau^2$ ($U_c = \langle U \rangle(y)$)

- $Re_\tau = 3600$, $Re_\theta = 13000$, present ZDES
- $Re_\tau = 2800$, Exp. Mathis et al. 2009
- - $Re_\tau = 3900$, Exp. Marusic et al. 2010

➤ Power Spectral Density estimation: **Welch's** method

➤ Time signal duration: $1155 \delta_0 / U_\infty$

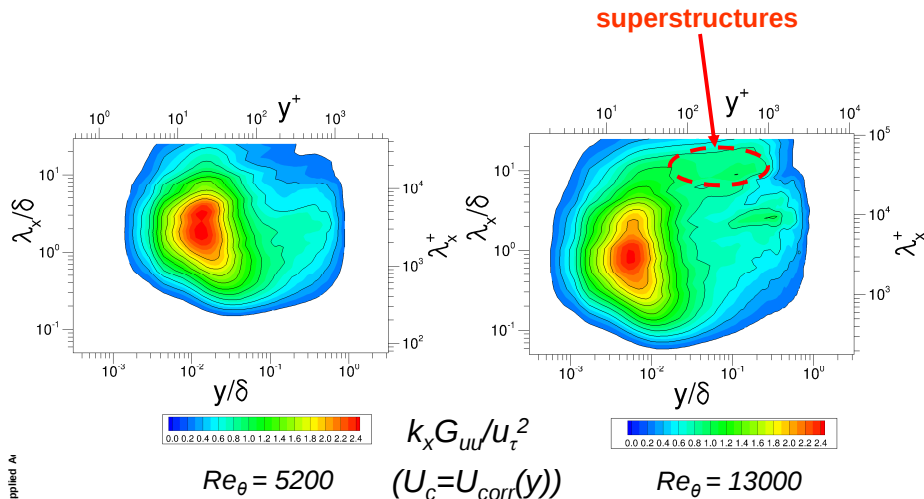
➤ **Taylor's** hypothesis
 $2\pi f = -k_x U_c$

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Streamwise PSD of u' : Reynolds number effect



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Analysis of mean skin friction: FIK identity

- Contribution of the superstructures to C_f ?

mean skin friction coefficient $C_f = \frac{\tau_w}{\frac{1}{2} \rho U_\infty^2}$

$\tau_w = \mu \frac{\partial \langle u \rangle}{\partial y} (y=0)$

- **FIK identity:** [6] Fukagata, K., Iwamoto, K. & Kasagi, N., Contribution of Reynolds stress distribution to the skin friction in wall-bounded flows, *Physics of Fluids*, 2002, 14, L73

- Mean streamwise momentum equation, zero pressure gradient:

$$\frac{\partial \langle u \rangle}{\partial t} + \overline{U_x} = \frac{\partial}{\partial y} \left(\nu \frac{\partial \langle u \rangle}{\partial y} - \langle u'v' \rangle \right) \quad \overline{U_x} = \frac{\partial}{\partial x} \left(\langle u \rangle^2 \right) + \frac{\partial}{\partial y} \left(\langle u \rangle \langle v \rangle \right) - \nu \frac{\partial^2 \langle u \rangle}{\partial x^2} + \frac{\partial}{\partial x} \left(\langle u'^2 \rangle \right)$$

- 3 integrations by parts over y later...

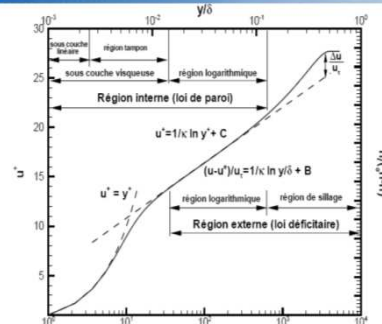
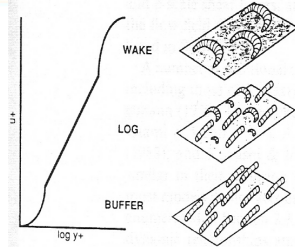
$$C_f = C_{f,1} + C_{f,2} + C_{f,3} \quad C_{f,2} = -4 \int_0^1 \frac{\langle u'v' \rangle}{U_\infty^2} \left(1 - \frac{y}{\delta} \right) d \left(\frac{y}{\delta} \right)$$

- Reynolds shear stress distribution:

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Grid requirements



RANS grid requirements:

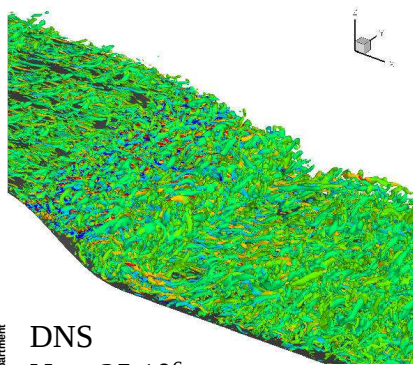
- $y^+ < 1$: $f(Re)$, typically $\Delta y \sim 10^{-5} - 10^{-6} m$ in aeronautical applications
- at least $N_y \sim 30$ points in δ , $d\delta/dx \sim 1 cm/m$
- $y_{i+1}/y_i < 1.1 \rightarrow N_y$

	Δx^+	Δy^+	Δz^+
LES	50	1	12
DNS	6	0.5	6

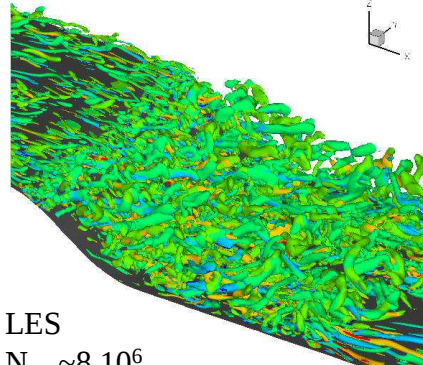
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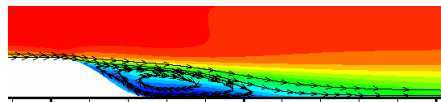
Separated flow over a S-shaped duct



DNS
 $N_{xyz} \sim 25 \cdot 10^6$



LES
 $N_{xyz} \sim 8 \cdot 10^6$



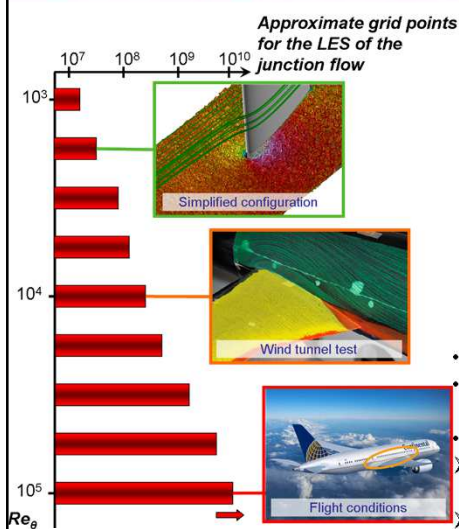
RANS
 $N_{xyz} \sim 2 \cdot 10^4$

(Courtesy of J.Dandois, ONERA)

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Towards Wall turbulence simulation at High Reynolds number. (flows of category III)



(F.Gand, PhD, ONERA)

Description of the present LES:

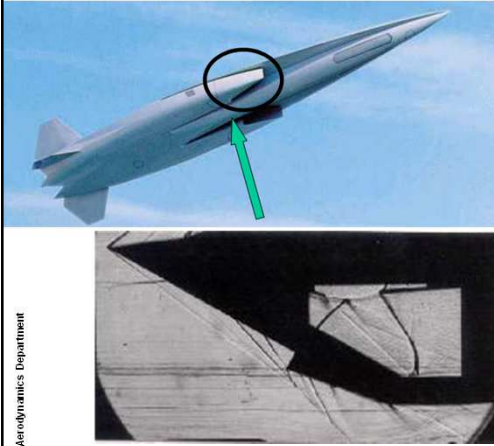
- $Re_\theta = 2100$. $Re_c = 3 \cdot 10^5$ $M = 0.15$.
- $N_{xyz} = 65 \cdot 10^6$. $\Delta t = 0.5 \mu s$
- 8 NEC-SX8 cores.
- 20000h CPU $\rightarrow$ 80ms
- Synthetic Eddy Method (SEM) (Pamiès et al. Phys. of Fluids, 21, 2009, developed by ONERA)

- $Re_\theta = 2100$ very far from technical configurations
- "standard" ($\Delta x^+ = 50$ - $\Delta z^+ = 15$ -20) LES not reachable in a near future at realistic Re
- Ongoing work at ONERA:
 - broadening of the application area of ZDES by permitting the activation of LES inside the BL
 - ZDES acts as WMLES

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Interaction Onde de Choc-Couche Limite Turbulente



S.Deck / Applied Aerodynamics Department

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Interaction Onde de Choc-Couche Limite Turbulente



(Courtesy of Jean-Paul Dussauge, IUSTI, Marseille)

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Interaction Onde de Choc-Couche Limite Turbulente

Vaste Gamme d'échelles:

1. Épaisseur du choc: λ_{choc}
2. Échelle de Kolmogorov: η_K
3. Taille de la maille de calcul: Δx

- Simulation directe: $\Delta x \leq \lambda_{\text{choc}} \leq \eta_K$
- Simulation quasi-directe : $\lambda_{\text{choc}} \leq \Delta x \leq \eta_K$
- LES ou URANS: $\lambda_{\text{choc}} \leq \eta_K \leq \Delta x$

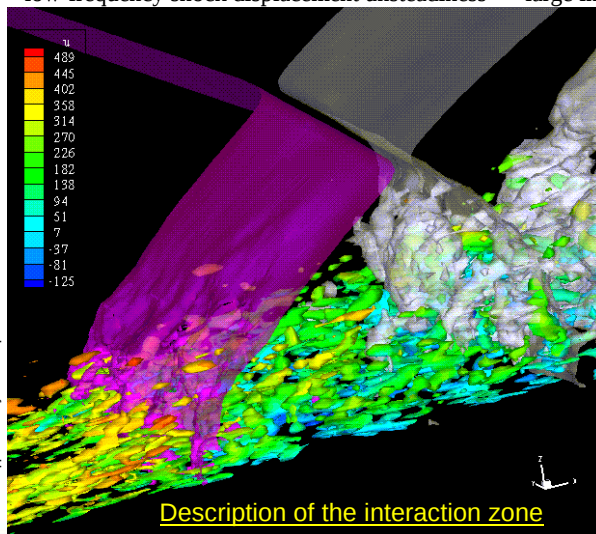
Coût d'une DNS

$$\text{computing time} \propto N_{xyz} \cdot N_t \propto \tilde{C} \cdot Re_L^3 \quad (\text{explicit schemes low CFL}, \dots)$$

$\tilde{C}$ is the cost of the algorithm expressed in $[s/\text{grid point}/\text{iteration}]$

Oblique-Shock/boundary layer interaction (Ma=2.3)

- supersonic intake (unsteady distortion)
- low-frequency shock displacement unsteadiness => large integration time



(LES, Courtesy of E. Garnier)

1. Grid requirements?
2. CPU cost ?